

# Preparation of activated carbons from some cellulosic wastes and their use in removal of oil spills from water bodies

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## Abstract

**Background/Objectives:** Preparing of activated carbons from agricultural wastes and testing its removal efficiencies of organic waste such as oil that oil spills on water bodies are harmful to the environment and humans.

**Methods/Statistical analysis:** The study involves the producing of activated carbon from wheat straw, uncooked and cooked corn cobs by using chemical activation method with 50 wt % phosphoric acid followed by carbonization in N<sub>2</sub> atmosphere at 500°C. Activated carbons were characterized by Fourier transform-infrared (FT-IR) spectroscopy and nitrogen adsorption/desorption isotherms.

**Finding:** Under certain process conditions, several active carbons with appropriate BET surface areas have been produced, reached 1343.75 m<sup>2</sup>/g and pore volumes 0.9106 cm<sup>3</sup>/g for cooked corn cob carbon.

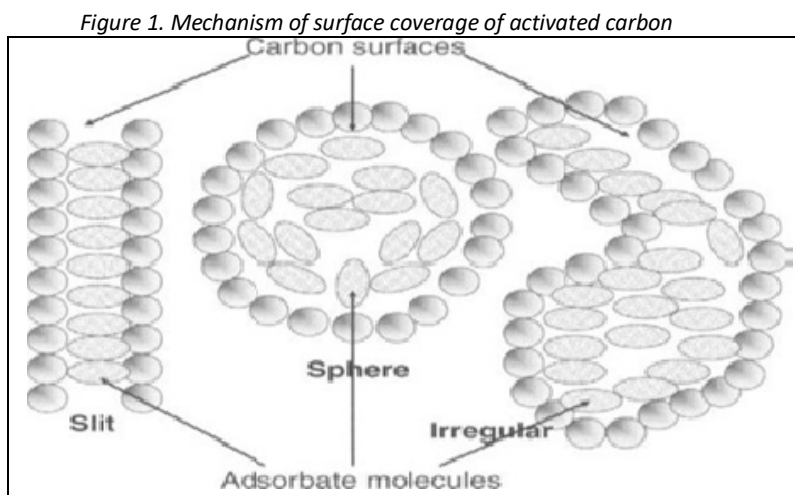
**Improvements/Application:** The best oil adsorption capacity was shown by activated carbon prepared from cooked corn cob 5.25g oil/g sorbent.

**Key words:** Oil spill, activated carbon, cellulosic wastes.

## 1. Introduction

Oil is one of the most important energies and raw material sources for synthetic polymers and chemicals worldwide. Whenever oil is explored, transported and stored and its derivatives are used, there is risk of spillage with the potential to cause significant environmental impact. Pollution by petroleum oils affects sea life, economy, tourism and leisure activities because of the coating properties of these materials. Oil spills harm the beauty of polluted sites; the strong odor can be felt miles away and the excessive growth of green algae alters sea color and the landscape [1]. From estimation, 3.2 million tons of oil is discharged into marine environment annually [2]. Crude oil spilt in the marine environment undergoes a wide variety of weathering processes, which include evaporation, dissolution, dispersion, photochemical oxidation, microbial degradation, agglomeration [1, 3]. One commonly used technique for remediation of petroleum-contaminated water is adsorption. Adsorption is a physical process wherein polluting chemicals adhere to the surface of a solid. Typically, most adsorbents have porous structure with many fine pores and occur in monolayer. A wide range of materials for water remediation have actually been employed in adsorbing oil and these include activated carbon [4]. Activated Carbon (AC) is widely used on an industrial scale as an adsorbent mainly in the purification/separation of liquids and gases and also as a catalyst and catalyst support. Furthermore, newer applications are ever emerging, particularly those concerning environmental protection and technological development [5]. Activated carbon is characterized by a vast system of pores of molecular size within the carbon particles. Activated carbon consists of non-planar layers of carbon (with some linearly or single bonded carbons). This makes up the entire carbon specimen and explains the existence of porosity and constitution of porosity over the entire carbon specimen. Figure 1 shows mechanism of surface coverage of activated carbon [6]. In addition, the properties of the resulting activated carbon will also be influenced by types of activating reagents, time, impregnation condition, carbonization temperature; inorganic impurities and others. The use of agricultural waste as activated carbon precursors has also been found to be renewable and relatively less expensive and ultimately could utilize the waste effectively into wealth. Any inexpensive material that has a high carbon and a low inorganic content can be utilized as a precursor for activated carbon productions. Subsequently, any lignocellulosic material can be used for activated carbon preparing [7].

The methods used for activated carbon synthesis are physical activation and chemical activation. In physical activation, the precursor is first carbonized in an inert atmosphere and then activated in a stream of carbon dioxide or steam; whereas for chemical activation, the precursor is impregnated with a dehydrating agent, usually zinc chloride or inorganic acids, prior to carbonization in an inert environment. In this study, chemical activation method is used due to the fact that the chemical activating agents play an important role in the carbonization process, in which they act as dehydration agents and minimize the formation of tar during carbonization. Furthermore, the temperature range used in chemical activation is lower in comparison to that used in physical activation. Phosphoric acid is selected as the activating agent instead of zinc chloride so as not to aggravate environmental pollution by contamination with zinc compounds and also it is easier to recover the carbon product during processing stage i.e. only rinsing with water is required [8].



## 2. Materials and methods

### 2.1. Materials

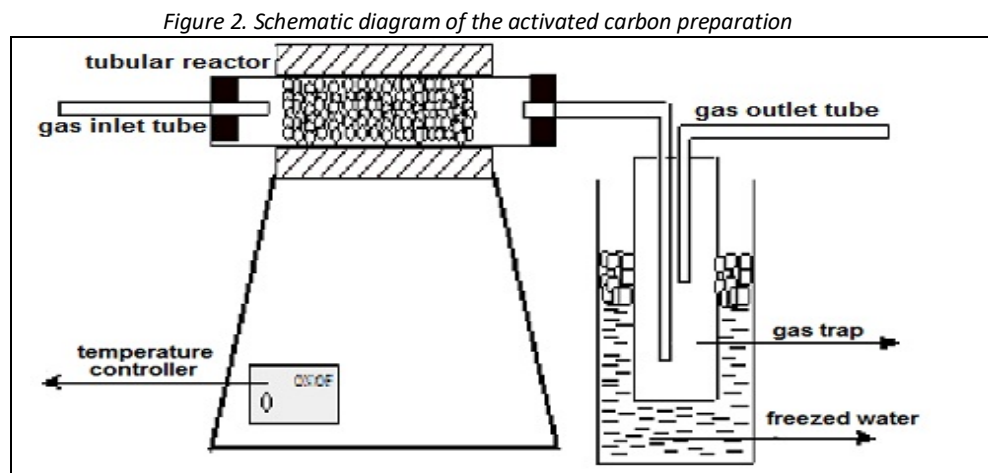
1. Wheat straw and corn cobs were collected from local resource (Aleppo-Syria).
2. Iranian crude oil (medium) was used as contaminant for water. The main physical properties of crude oil were summarized in Table 1. Phosphoric Acid with purity of 85% (Merck), gas N<sub>2</sub> with purity of 99.995%.

*Table 1. Characteristic of investigated oil*

Properties	Crude Oil
Pouring Point, °C	-16
Density, g/cm <sup>3</sup>	0.855
Viscosity, CST	5.5
Sulfur content, wt. %	1.45
Water content, ppm	<0.05
Salt content, ppm	50
Sediment, ppm	<0.1

### 2.2. Activated carbon preparation by chemical activating with phosphoric acid

Wheat straw, cooked and uncooked corn cobs which used for preparation of activated carbons were obtained locally. The precursors were dried overnight in an oven at 105 °C. The dried plant samples were cut and sieved to desired mesh size (1–2 mm). The activated carbons were prepared by impregnating the dried precursor with 50wt % H<sub>3</sub>PO<sub>4</sub> with ratio of 1:2.5 for 72 hrs then filtrated and dried at 393 K. Then the products were loaded in a stainless steel vertical tubular reactor placed in a tube furnace and carbonized at 500 oC for 3hrs in absence of air and in flow of purified nitrogen (99.995%) at 80ml/min. The schematic diagram of the activated carbon preparation is shown in Figure 2 [5, 9].



The carbonized products were washed several times with hot water then cold bidistilled water until the pH value of the effluent reached 7, filtered and finally dried at 105 °C. The dried activated carbons were crushed and sieved to desired mesh size (90 μm). The obtained activated carbons were designed ASWSC, UCC, and CCC for wheat straw, cooked and uncooked corn cobs respectively.

### 2.3. Determination of dynamic oil adsorption capacity

A 500 ml sample of artificial sea water (3.5% NaCl) was placed in a 1 L glass beaker. 40g of oil was added to the beaker. The beaker containing crude oil and artificial sea water was mounted in a shaking apparatus; 4g of a sorbent material was added to the beaker, which was shaking for 15 min at 150 cycles/ min.

The oil content was weighed after a 30 seconds drain period. Oil content of the sorbent was analyzed according to ASTM F 726-99 and calculated from the equation.

$$\text{Oil absorbency ((g oil)/ (g sorbent))} = (S_s - S_0)/S_0$$

$S_0$  = initial dry adsorbent weight (g).

$S_s$  = weight of adsorbent samples at end of oil test (g).

This test was performed at  $23 \pm 4^\circ\text{C}$ . And all oil absorbency was measured three times and an average value was used [1, 10].

### 2.4. Determination of textural properties

The pore structural characteristics of the as-prepared activated carbons were determined by nitrogen adsorption at 77 K using a nitrogen sorption/desorption measurements. Prior to the analysis, the sample was degassed for 3 h under vacuum at 573 K. The sample was transferred to the analysis system where it was cooled in liquid nitrogen. Analysis was carried out at 77 K to obtain the nitrogen adsorption isotherm. The SBET was calculated by the BET (Brunauer–Emmett–Teller) equation. The total pore volume was estimated to be the volume of liquid N<sub>2</sub> adsorbed at a relative pressure of 0.95. The mean pore radius ( $r_a$ ) was calculated from the equation (2) [11].

$$(2) \quad r_a = (2000 V_p)/S_{BET}$$

$V_p$  = total pore volume (ml/g).

$S_{BET}$ : surface area (m<sup>2</sup>/g).

## 3. Results and discussion

### 3.1. Oil adsorption capacity

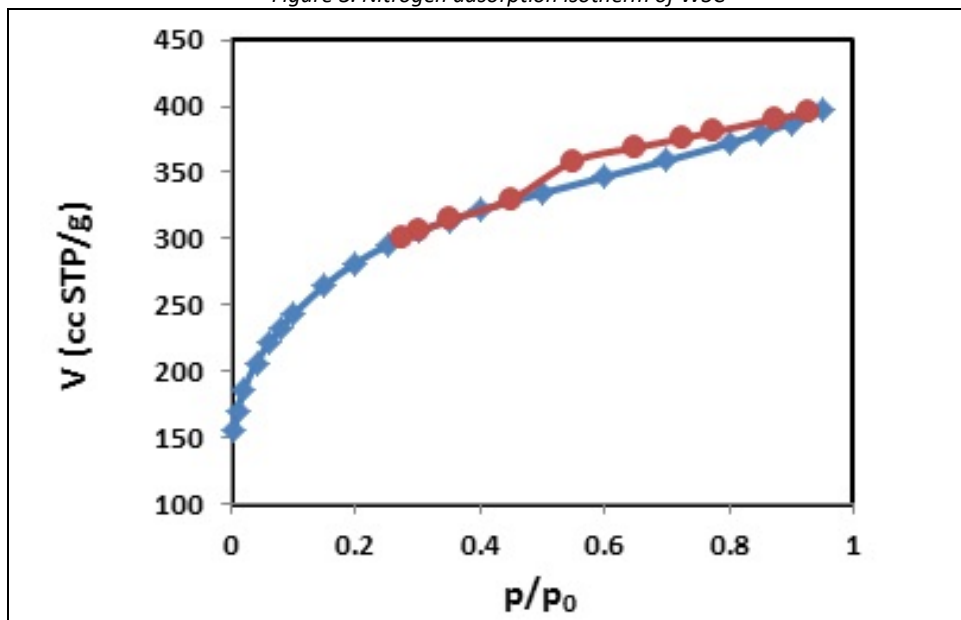
Table 2 shows the oil adsorption capacity of the activated carbons prepared from the three agricultural wastes (wheat straw, cooked and uncooked corn cobs). The best oil adsorption capacity was from activated carbon prepared from cooked corn cob 5.25g oil/g sorbent.

Table 2. Oil adsorption capacity

Adsorption Material	wsc	ucc	ccc
Adsorption Value (g <sub>oil</sub> /g <sub>sorbent</sub> )	2.22	4.10	5.25

3.1. Brunauer-Emmett-Teller (BET) equation

Figure 3. Nitrogen adsorption isotherm of WSC



Figures 3-5 show the N<sub>2</sub> adsorption-desorption isotherms of the prepared activated carbons. These adsorption isotherms give information about the porous structure of the adsorbent. As can be seen, the adsorption isotherms are between a type IV and type I in according to the IUPAC classification. The isotherms indicate that the prepared activated carbons have both micro and Mesopores [11].

Figure 4. Nitrogen adsorption isotherm of UCC

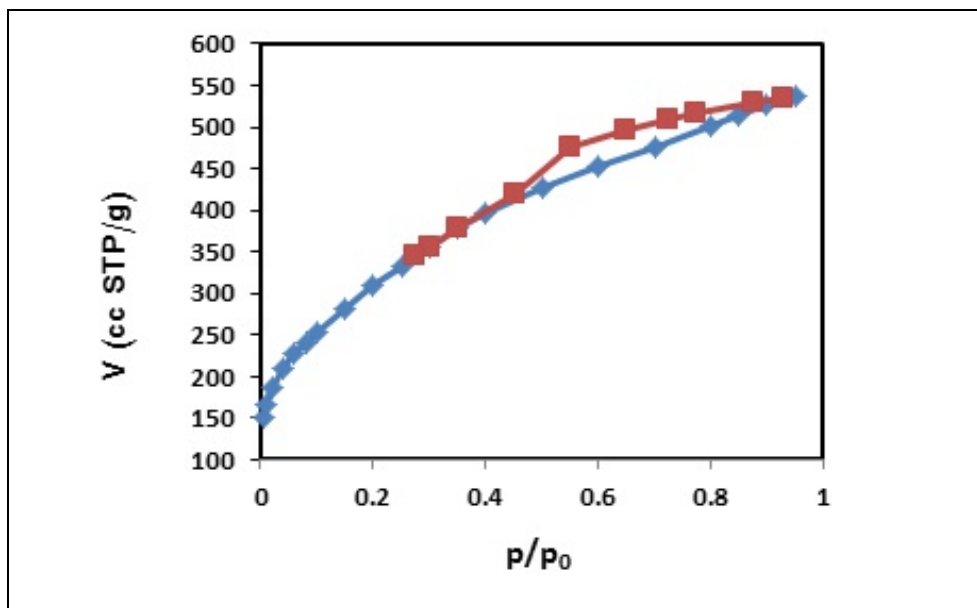
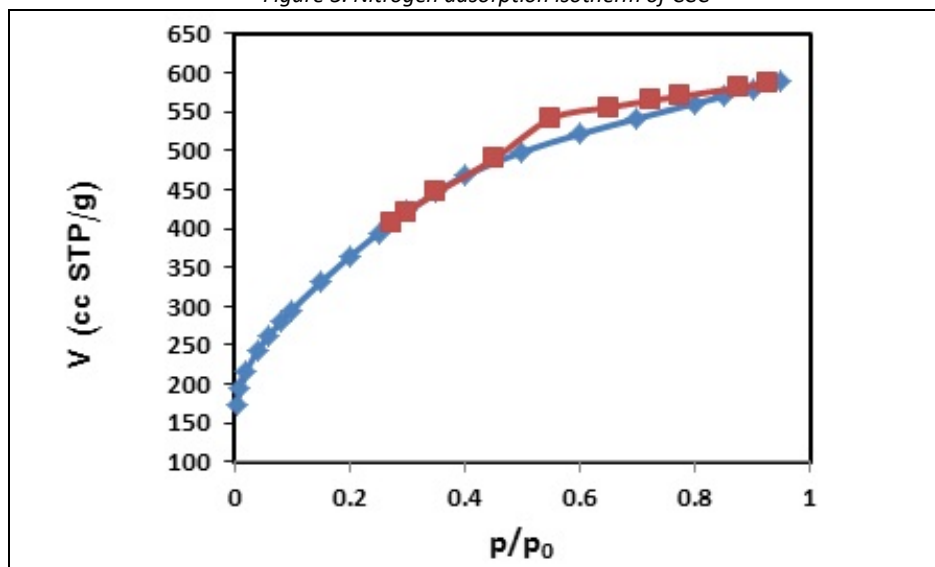


Figure 5. Nitrogen adsorption isotherm of CCC



The textural characteristics (surface area, total pore volume and mean pore radius) of the prepared activated carbons are summarized in Table 3.

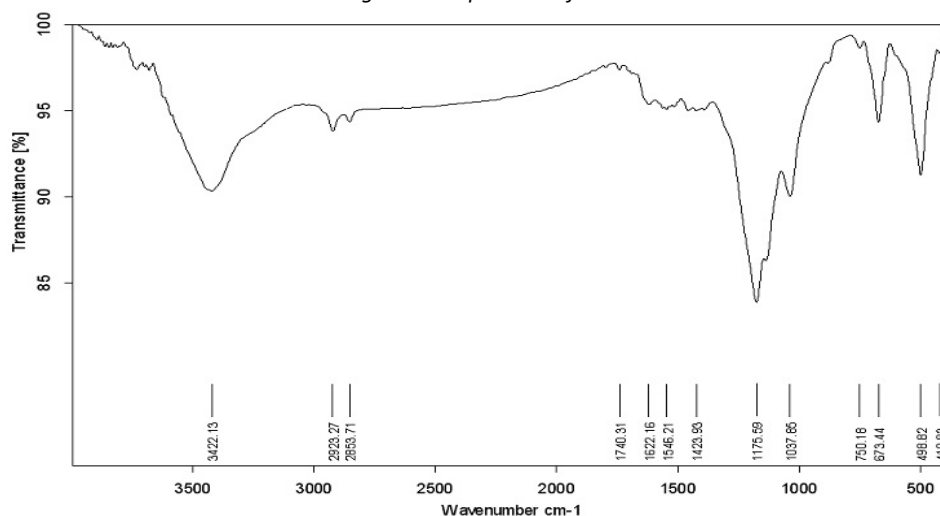
Table 3. Porosity data of the activated carbons

Sample	S <sub>BET</sub> surface area (m <sup>2</sup> /g)	V <sub>p</sub> Total pore volume (cm <sup>3</sup> /g)	r <sub>a</sub> (nm)
wsc	951.39	0.6133	1.289
ucc	1129.00	0.8308	1.471
ccc	1343.75	0.9106	1.355

### 3.2. IR spectrums

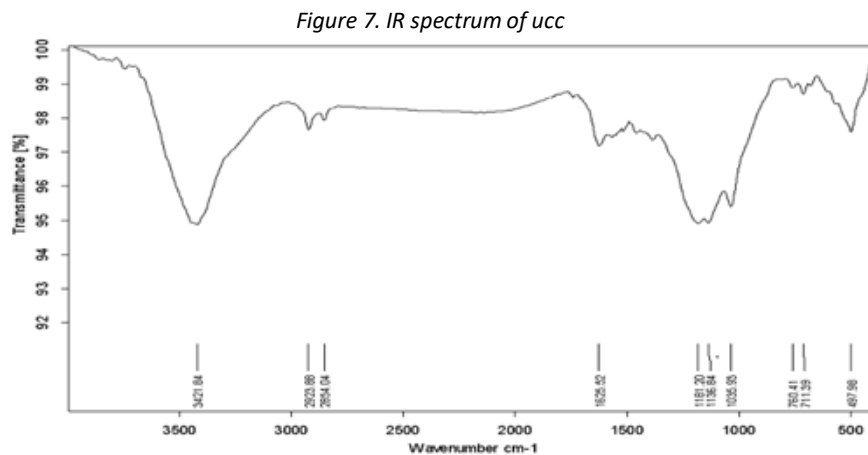
Infrared spectroscopy provides information on the chemical structure of the activated carbons. Figures 6-8 show the FTIR spectra of the synthetic carbons obtained by phosphoric acid activation from wheat straw, uncooked and cooked corn cobs.

Figure 6. IR spectrum of wsc

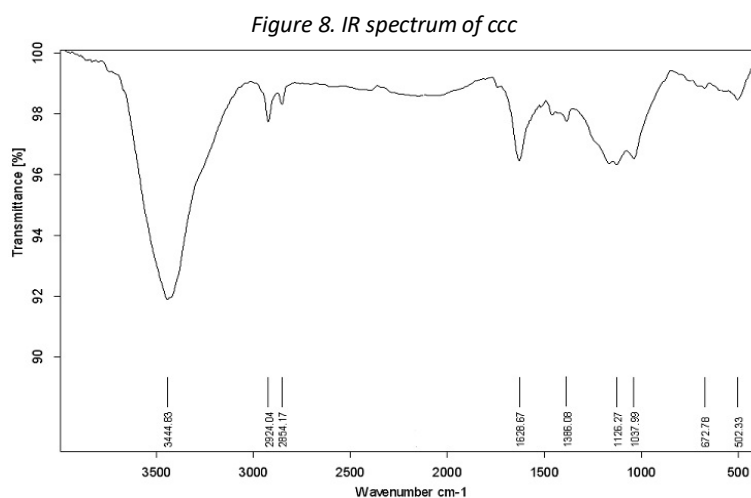


All spectra show a wide transmittance band at 3420–3450 cm<sup>-1</sup>. This band can be assigned to the O–H stretching mode of hydroxyl groups and adsorbed water. The position and asymmetry of this band at lower

wave numbers indicate the presence of strong hydrogen bonds. The FTIR spectrum of synthetic carbons shows absorption bands due to aliphatic (2920 and 2850  $\text{cm}^{-1}$ : C–H stretching in –CH–; 1450  $\text{cm}^{-1}$ : –CH– deformation). The bands near (750)  $\text{cm}^{-1}$  are due to out-of-plane deformation mode of C–H for different substituted benzene rings. The small band at about 1700  $\text{cm}^{-1}$  is usually assigned to C=O stretching vibrations of ketones, aldehydes, lactones or carboxyl groups [5].



The spectra of the prepared activated carbons also show a strong band nearby (1620)  $\text{cm}^{-1}$  due to C–C vibrations in aromatic rings. Broad band at 1000–1300  $\text{cm}^{-1}$  is usually found with oxidized carbons and has been assigned to C–O stretching in acids, alcohols, phenols, and ethers and/or esters groups [9]. Nevertheless, it is also a characteristic of phosphorous and phosphor carbonaceous compounds present in the phosphoric acid activated carbons [13]. Assignment in this region is difficult because absorption bands are overlapped. The peak at 1190–1200  $\text{cm}^{-1}$  may be also assigned to the stretching mode of hydrogen-bonded P=O, to O–C stretching vibrations in P–O–C (aromatic) linkage and to P=OOH [5].



#### 4. Conclusions

In summary, we successfully prepared a well-developed porous texture of activated carbons by using natural waste of (wheat straw, uncooked and cooked corn). It was found that these agricultural wastes can serve as potential source for manufacturing activated carbons with a high surface area, which can operate as a capable adsorbent for water treatment. The best BET surface area was for activated carbon prepared from cooked corn cob 1343.75 $\text{m}^2/\text{g}$ . The best oil adsorption capacity was shown by activated carbon prepared from cooked corn cob 5.25 g oil/g sorbent.

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## 6. Reference

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